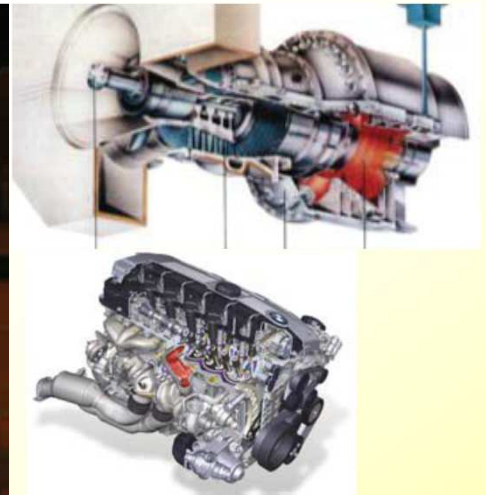


# ERA-NET Bioenergy project “EnCat”

Enhanced catalytic fast pyrolysis of biomass for maximum production of high quality biofuels



**Thomas Brunner**

**BIOS BIOENERGIESYSTEME GmbH**

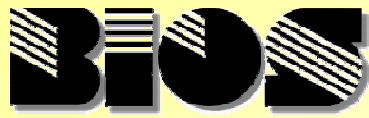
**Hedwig-Katschinka-Straße 4, A-8020 Graz, Austria**

**TEL.: +43 (316) 481300; FAX: +43 (316) 4813004**

**E-MAIL: [office@bios-bioenergy.at](mailto:office@bios-bioenergy.at)**

**HOME PAGE: <http://www.bios-bioenergy.at>**



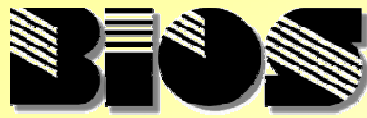


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Hedwig-Katschinka-Straße 4, A-8020 Graz

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## EnCat key data and project consortium (I)

**EnCat**      **Enhanced catalytic fast pyrolysis of biomass for maximum production of high quality biofuels**

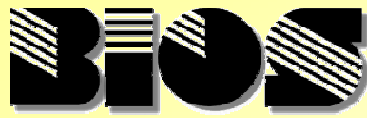
**Duration: 42 months (project start: 02/2017)**

**The project is carried out in the core of the ERA-NET Bioenergy programme “10<sup>th</sup> Joint Call for Research and Development Proposals of ERA-NET Bioenergy”**

### Partner from Austria



**BIOS BIOENERGIESYSTEME GmbH**



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## EnCat key data and project consortium (II)

### Partners from the Netherlands



**University of Twente** (project coordinator)



**Alucha Management B.V.**



**OPRA Turbines International BV**

### Partners from Sweden



**KTH Kungliga Tekniska högskolan**



**RISE Research Institute of Sweden**

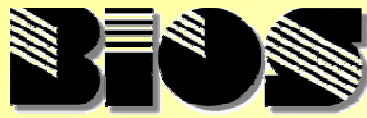
### Partners from Poland



**ICHPW Institute for Chemical Processing of Coal**



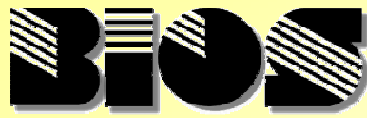
**HIG Polska Sp. z o.o.**



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## Background and intention (I)

- **Fast pyrolysis of biomass** is one of the most promising ways to directly generate liquid fuels from biomass
  - However, the produced **pyrolysis oil** may have **several drawbacks** which suppress its application for power and heat generation or transportation fuels
    - high oxygen content
    - high water content
    - high contents of water-soluble acids
- which affect negatively the**
- acidity (corrosion effects)
  - miscibility with petroleum-based fuels (separation of fractions)
  - chemical stability (aging)
  - viscosity
  - energy density

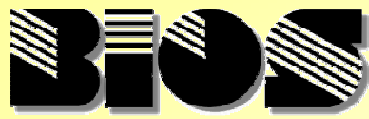


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## Background and intention (II)

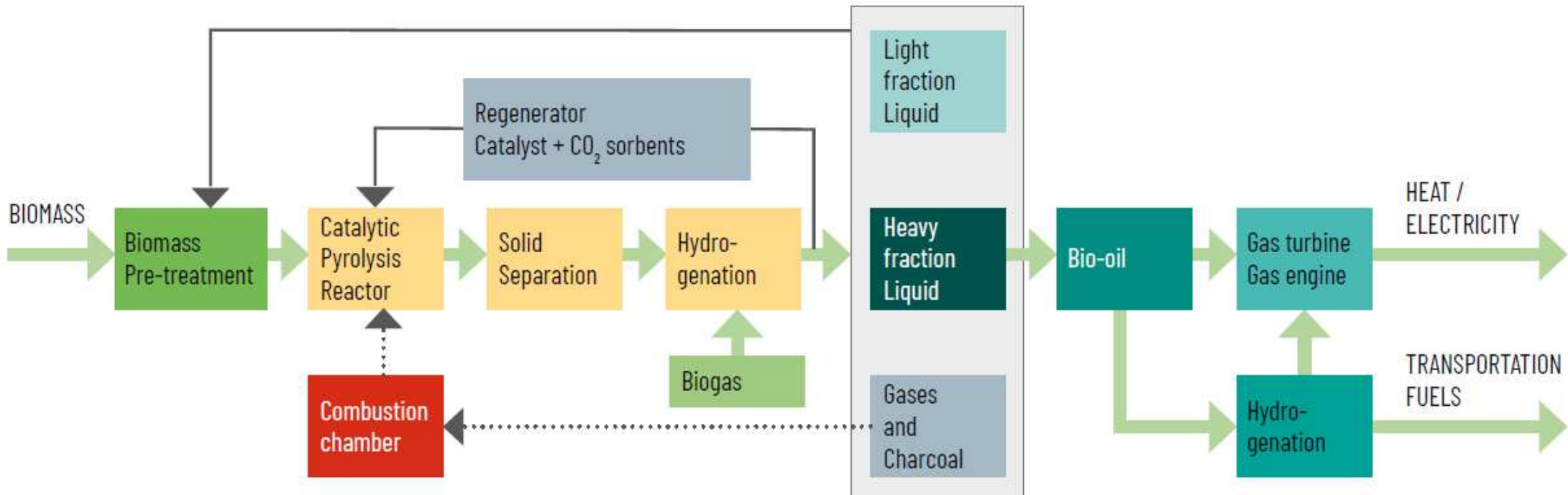
- The **Enhanced Catalytic Pyrolysis (EnCat)** project investigates a new concept for the production of high-quality bio-oil
- The **EnCat concept** consists of the following components
  - A novel **biomass pre-treatment** step to make the concept suitable for both woody biomass and biomass residues from agriculture
  - Biomass **pyrolysis** in a reactor making use of **deoxygenation catalysts**
  - Simultaneous **CO<sub>2</sub> capture with sorbents** and via the water-gas-shift reaction **in-situ production of hydrogen**
  - After cleaning, the oil vapours will be **mildly hydrogenated** to produce a high-quality bio-oil.
  - Utilisation of the bio-oil in **gas engines** and a **gas turbines**
  - Further upgrading by a new method of **downstream hydrogenation**

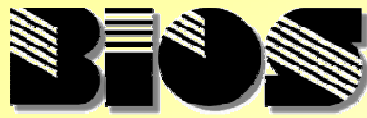




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## EnCat concept



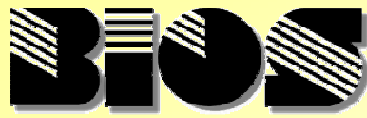


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## Overall objectives

- Development of a new concept for the production of biofuels based on an enhanced catalytic flash pyrolysis process including deoxygenation and hydrogenation for the high-yield production of high-quality bio-oil from both woody and residual biomass streams
- To test the high-quality oil in gas turbines and diesel engines for the production of heat and power
- To further increase the applicability of the bio-oil as transportation fuel by downstream hydrogenation
- To evaluate the new concept from biomass to biofuels with respect to sustainability and techno-economic feasibility

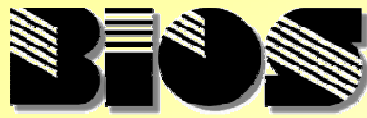




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## Scientific objectives (I)

- Get insight in the **catalytic pyrolysis** mechanisms of different biomass streams (woody biomass, agricultural residues)  
➔ *University Twente, KTH*
- To develop a **leaching process** for the biomass feedstock in order to remove alkaline and alkaline earth metals (AAEMs) and to optimize this process  
➔ *BIOS*
- Understand and develop the application of **CO<sub>2</sub> sorbents** in catalytic pyrolysis reactors for in-situ production of hydrogen  
➔ *University Twente*
- Development of a **downstream hydrogenation** process for the production of bio-oil with low oxygen contents that can be used as transportation fuel  
➔ *ICHPW*



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## Scientific objectives (II)

- Improve **atomization** and **combustion** of bio-oil in **gas turbines** and to optimize existing gas turbines for (catalytic) pyrolysis oil applications with low emissions and high efficiencies via experimental research and numerical (CFD) simulations  
➔ *OPRA, BIOS, University Twente*
- To investigate bio-oil combustion in **gas engines**  
➔ *ICHPW*
- To design a **full-scale plant** based on enhanced catalytic pyrolysis and to develop a roadmap for further commercialization  
➔ *Alucha*
- Evaluation of the new concept from biomass to biofuels with respect to sustainability and techno-economic feasibility  
➔ *RISE, BIOS*

## Selected results – Biomass pre-treatment – BIOS (I)

### Objectives

- High contents of **alkaline and alkaline earth metals** (AAEM – Ca, Mg, K and Na) in agricultural biomass feedstocks cause problems during pyrolysis (reduced oil and sugar yield)
- Development and lab-scale test of **leaching** methods with the aim to **reduce the AAEM contents** of agricultural biomass feedstocks to make them applicable for the pyrolysis process

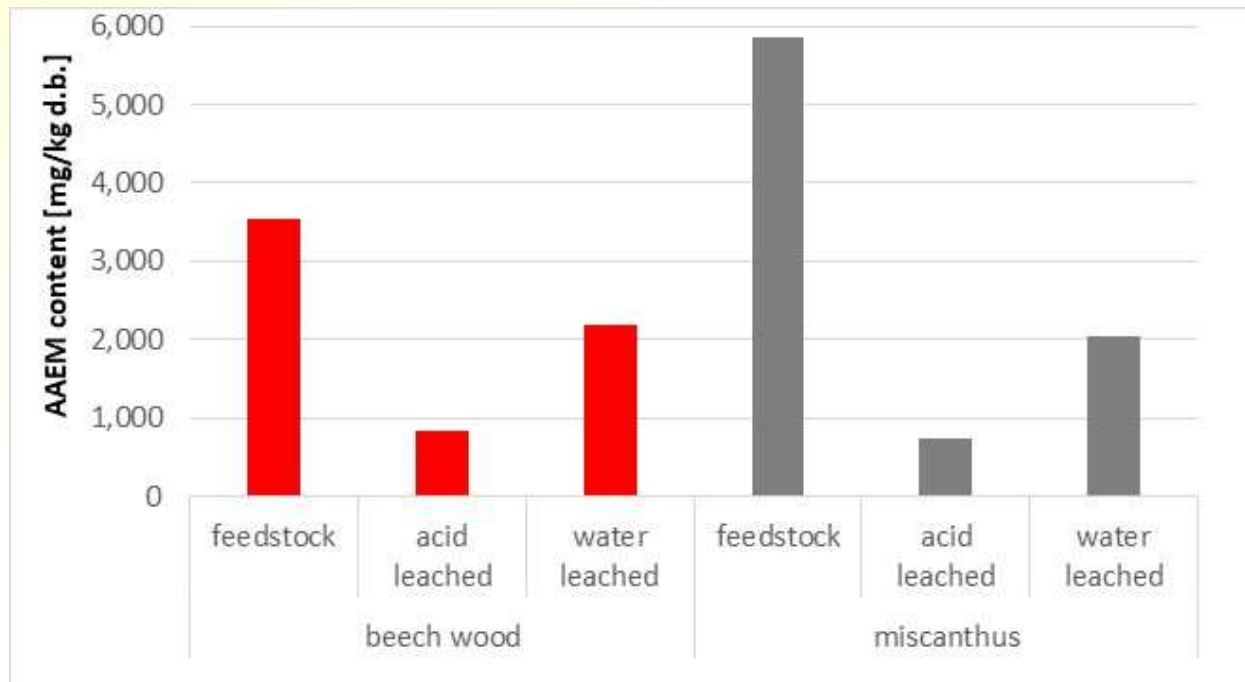
### Methodology

- Leaching tests of woody and agricultural biomass with acids and water
- Comprehensive parametric study regarding the influence of
  - acidity
  - temperature and
  - residence time
  - fuel to leaching liquid ratioon the leaching efficiency



### Preliminary results

- **Leaching of woody biomass (beech wood)**
  - with acids: 75% AAEM reduction
  - with water: 33% AAEM reduction
- **Leaching of agricultural biomass (miscanthus)**
  - with acids: 85% AAEM reduction
  - with water: 60% AAEM reduction



Leaching at mild conditions:  
30°C, 30 minutes residence time,  
acid leaching: 1% acetic acid in water

➔ **Even when leaching with water the AAEM contents of miscanthus can be reduced below the AAEM level of beech wood**

## Objectives

- Experimental study of catalytic fast pyrolysis with MCM-41 and HZSM-5 zeolite catalysts
- Improve the bio-oil quality
- Determine the effects of catalysts on the bio-oil quality

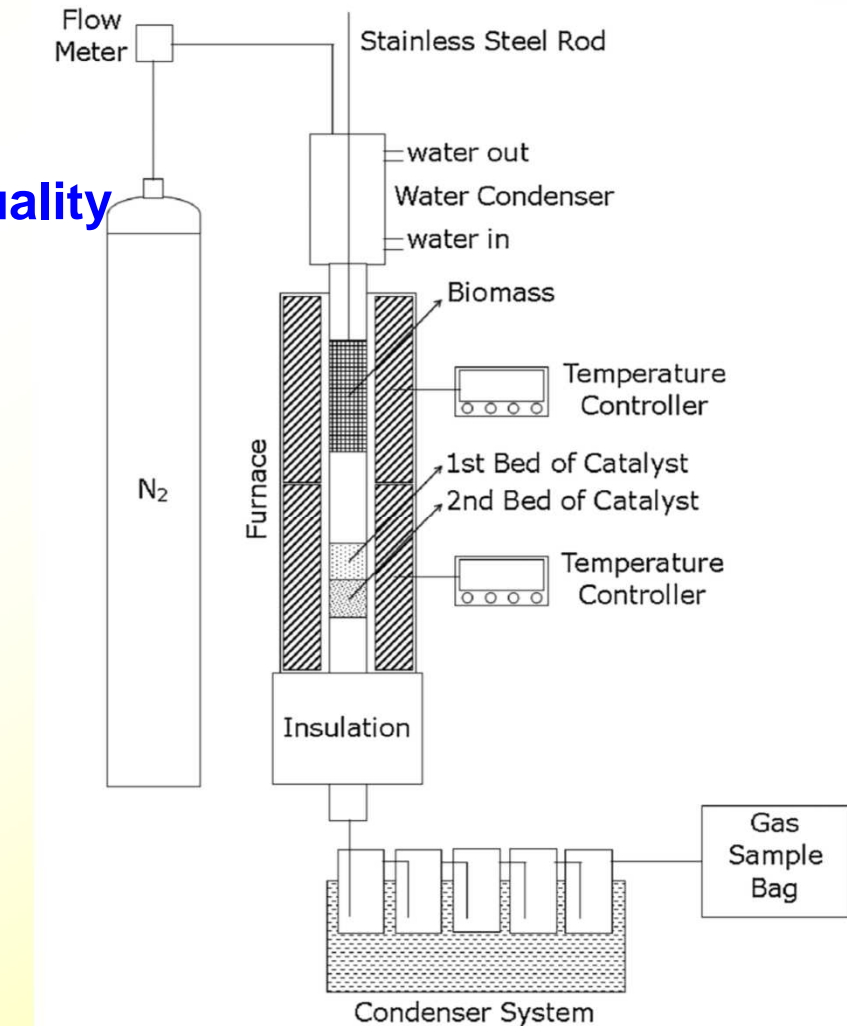
## Methodology

Reactor heated up to the target temperature for the catalysts (500°C)

The evolved volatiles from the sample are passed directly to the ex-situ beds containing catalysts

The ratio of MCM-41 and HZSM-5 zeolite catalyst was altered to give the required ratio

The ratio of sample to catalysts was 1:1



### Results for different catalyst ratios of H-ZSM-5 and Al-MCM-41

Experiment	Element (wt.%)				Deoxygenation degree (%)	HHV Dulong (MJ/kg)	Heavy Oil (g)	HHV Dulong (MJ)	Relative Energy
	C	H	O	N					
<b>Non-catalytic</b>	47,25	7,91	43,10	0,50	1,60	19,55	57,95	1,13	100%
<b>H-ZSM-5</b>	73,50	7,79	21,00	0,61	52,05	32,28	7,08	0,23	20%
<b>HA 7:1</b>	74,90	8,00	15,00	0,59	65,75	34,15	5,66	0,19	17%
<b>HA 3:1</b>	82,05	8,37	8,60	0,50	80,37	38,26	4,25	0,16	14%
<b>HA 2:1</b>	80,00	8,11	10,30	0,61	76,48	36,89	3,54	0,13	12%
<b>HA 1:1</b>	84,20	8,24	6,70	0,62	84,70	39,15	2,83	0,11	10%
<b>Al-MCM-41</b>	85,60	8,20	4,80	0,63	89,04	39,91	1,42	0,06	5%

Deoxygenation degree (%) =  $(1 - (O\text{-biooil}/O\text{-biomass})) \times 100$

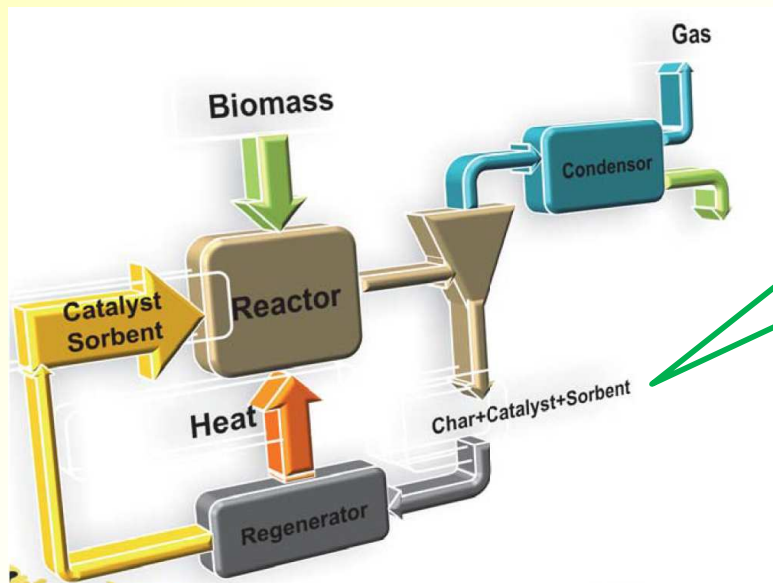
HHV Dulong =  $338.2C + 1442.8(H - (O/8))/1000$



## Enhanced catalytic pyrolysis – UT (I)

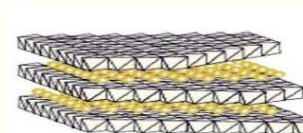
### Aim of the work:

- Improve Quality of pyrolysis oil (reduce acidity i.e., carboxylic acids)



- **Catalyst:** Deoxygenation Reactions (e.g., remove acids)
- **Sorbent:** Capture  $\text{CO}_2$  and shift equilibrium of WGS  $\text{CO} + \text{H}_2\text{O} \rightleftharpoons \text{CO}_2 + \text{H}_2$  (Exothermic Reaction) for in-situ hydrogen ( $\text{H}_2$ ) production

**Hydrotalcite**

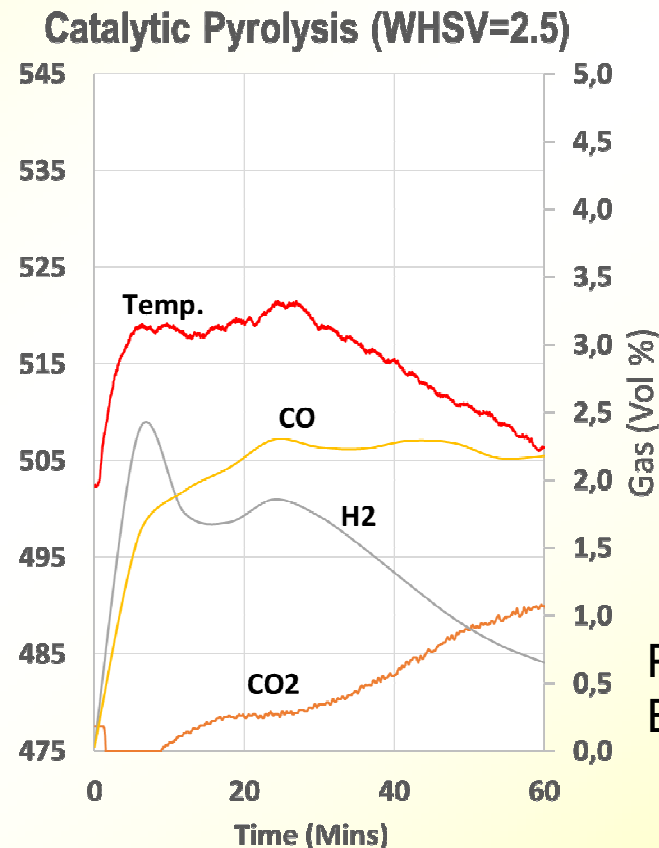
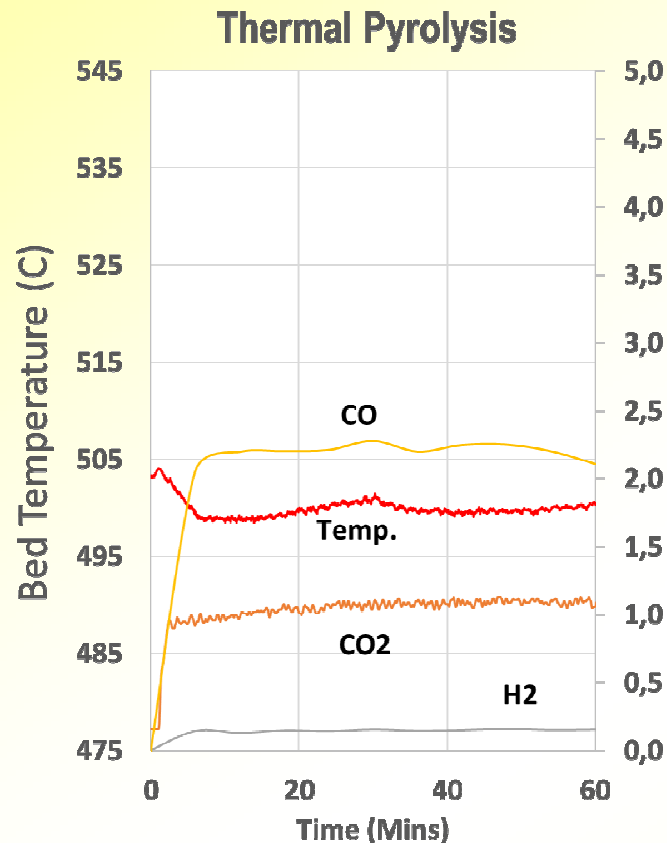


**Dolomite**



Hydrotalcite and Dolomite are selected due to their ability for both deoxygenation and  $\text{CO}_2$  sorption reactions

### Test results with Dolomite in a fluidized bed reactor

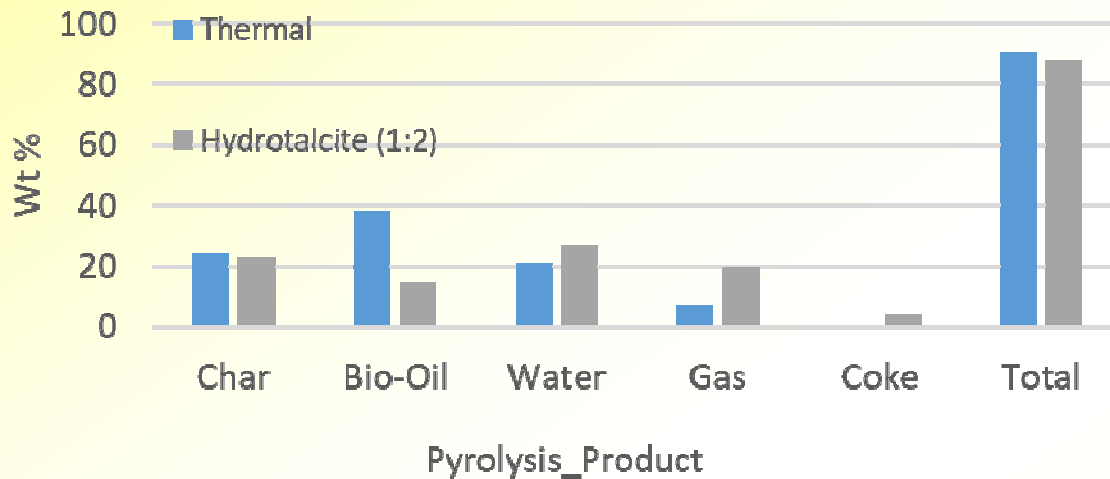


Pyrolysis Temperature: 500°C  
Experimental Time: 60 Min.

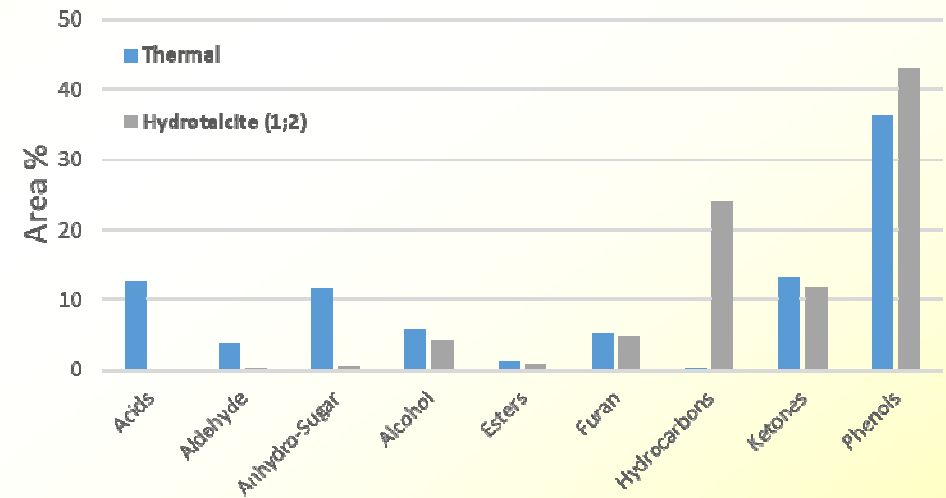
- Clear indication of equilibrium shift of WGS Reaction ( $\text{CO} + \text{H}_2\text{O} \rightleftharpoons \text{CO}_2 + \text{H}_2$ )
- **40.4%** bio-oil yield
- **5.74 %** of H in the feed converted to Hydrogen via water gas shift reaction

## Test results with Hydrotalcite

Mass Balance



Bio-Oil composition GC-MS (organic Phase)



- Minor increase in H<sub>2</sub> Production
- Increase in Hydrocarbon
- Elimination of Acids

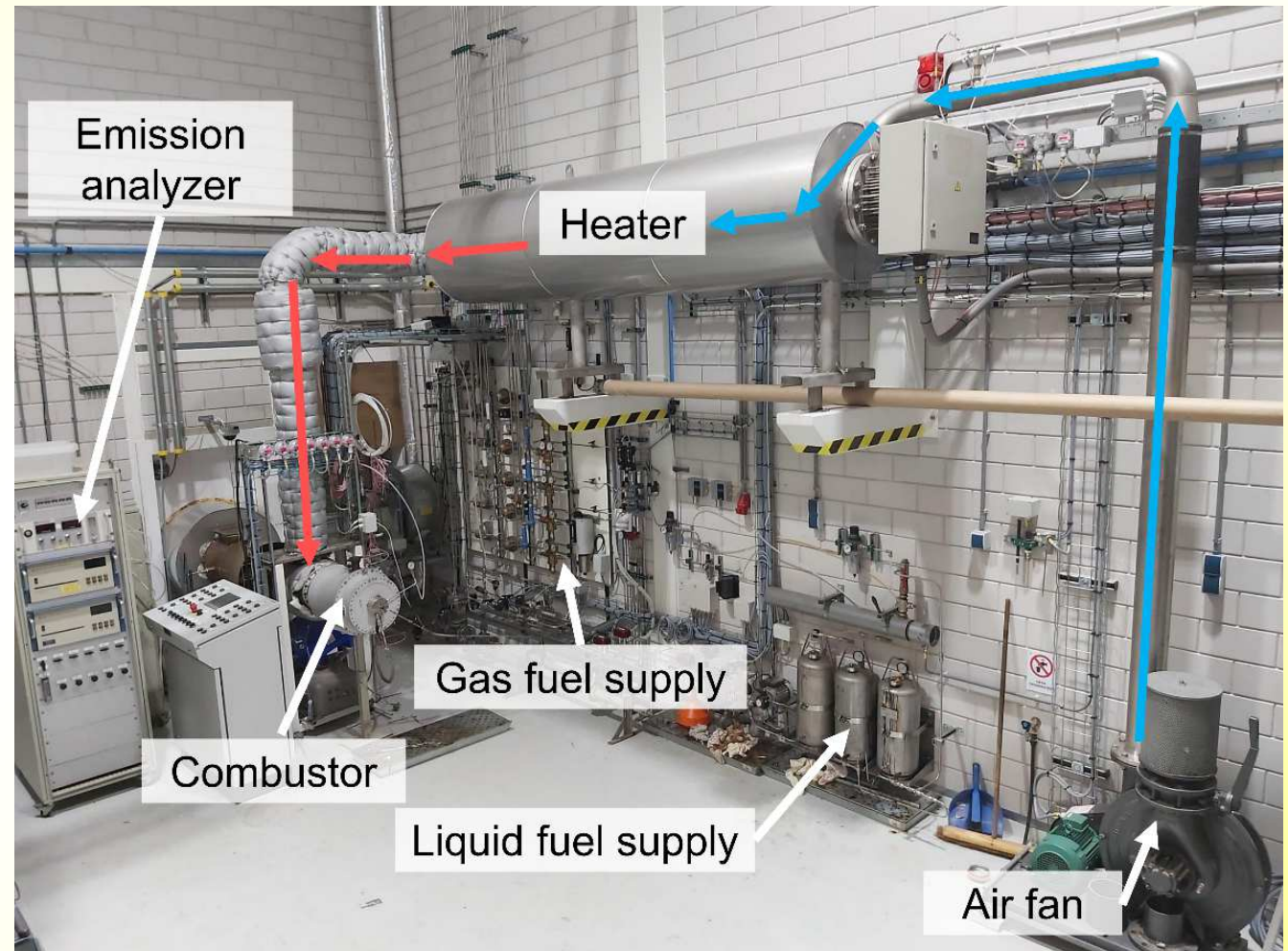


## Bio-oil combustion tests – OPRA (I)

### Full-scale gas turbine combustor tests at atmospheric conditions

#### Measurement of:

- Temperatures (inlet, outlet)
- Pressures
- Air and fuel mass flow
- Liner metal temperatures by thermochromic paint
- Emissions (CO, CO<sub>2</sub>, NO, NO<sub>2</sub>, O<sub>2</sub>)



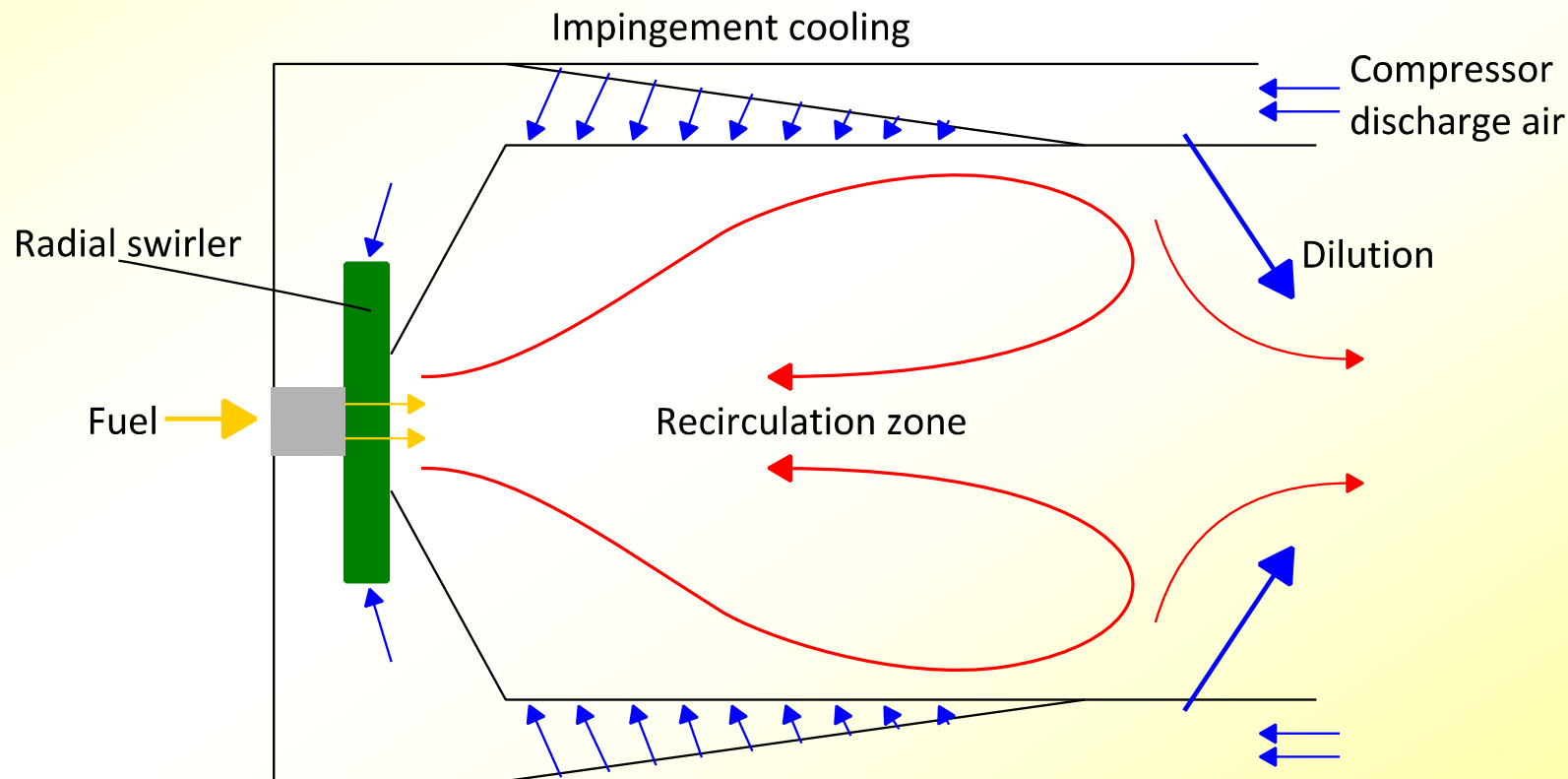
Atmospheric combustor test rig at OPRA



### Design of the OPRA 3C low calorific fuel combustor

#### 3C combustor\* designed for burning low-calorific gaseous and liquid fuels

- Diffusion type combustor
- Significantly larger volume than conventional combustor
- Impingement cooling



\*Patent US 8,844,260  
Low calorific fuel combustor  
for Gas Turbine

## Bio-oil combustion tests – OPRA (III)

### Wood pyrolysis oil successfully tested during the EnCat project by applying a new nozzle design

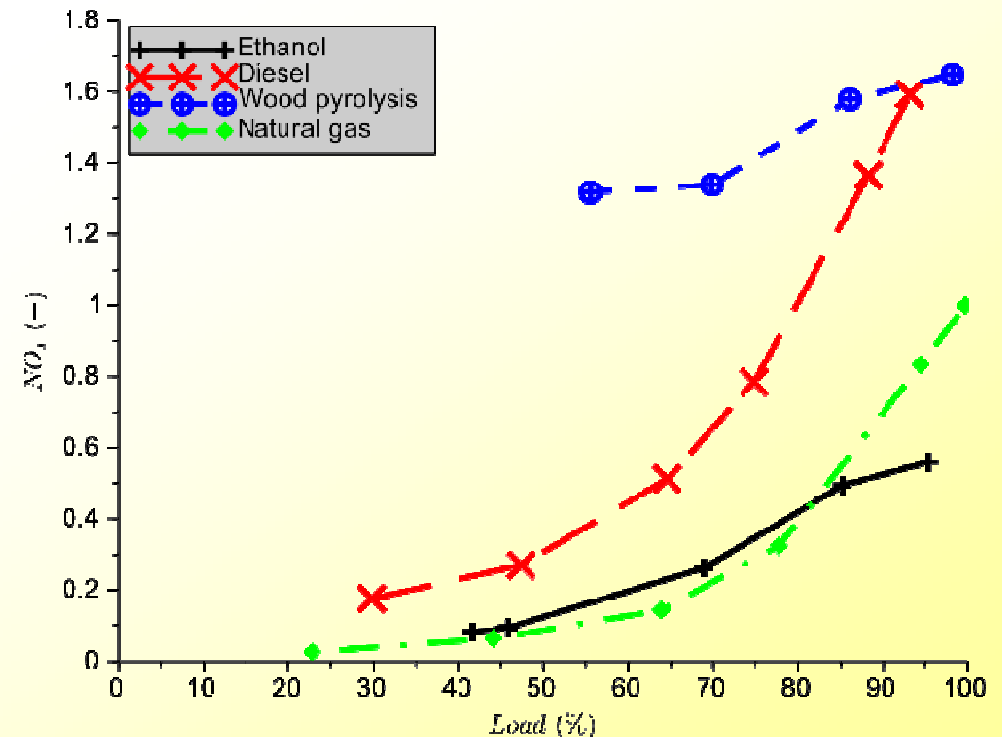
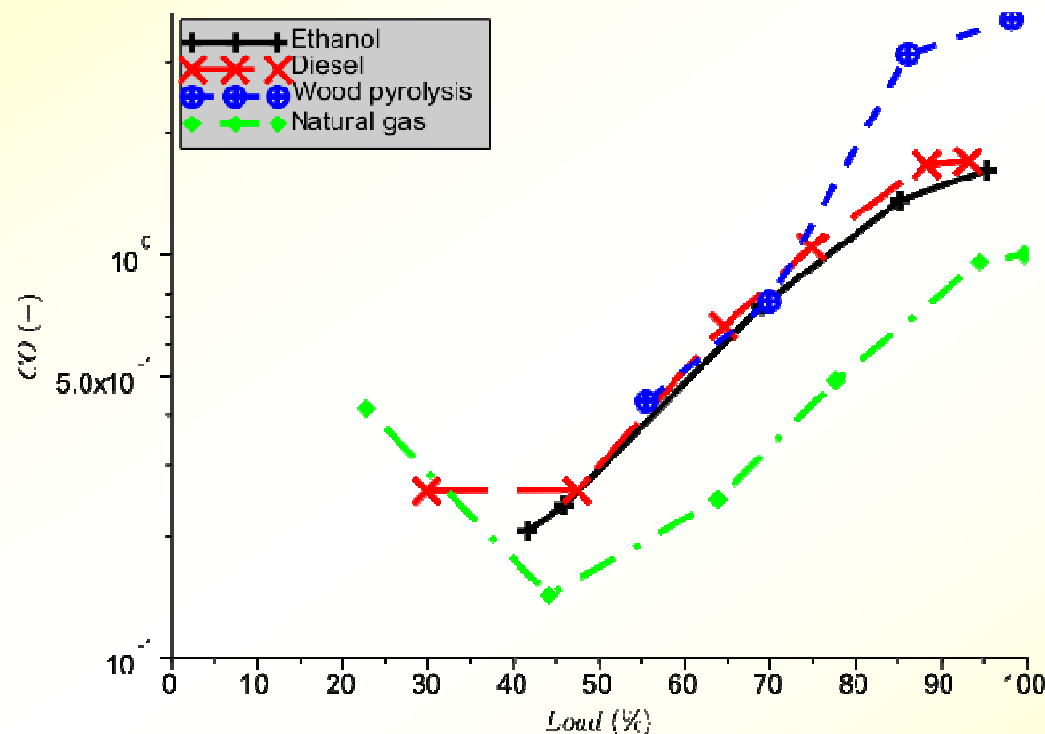
- Good atomization is a key parameter for operating liquid fuels
- High viscosity and polymerization at high temperatures make pyrolysis oil atomization challenging
- New nozzle has been developed by OPRA which allows stable operation with 100% wood pyrolysis oil over wide load range
- Nozzle has been successfully tested in the atmospheric combustor test rig with multiple fuels
- CFD simulations of BIOS and UT for further combustor optimisation are ongoing





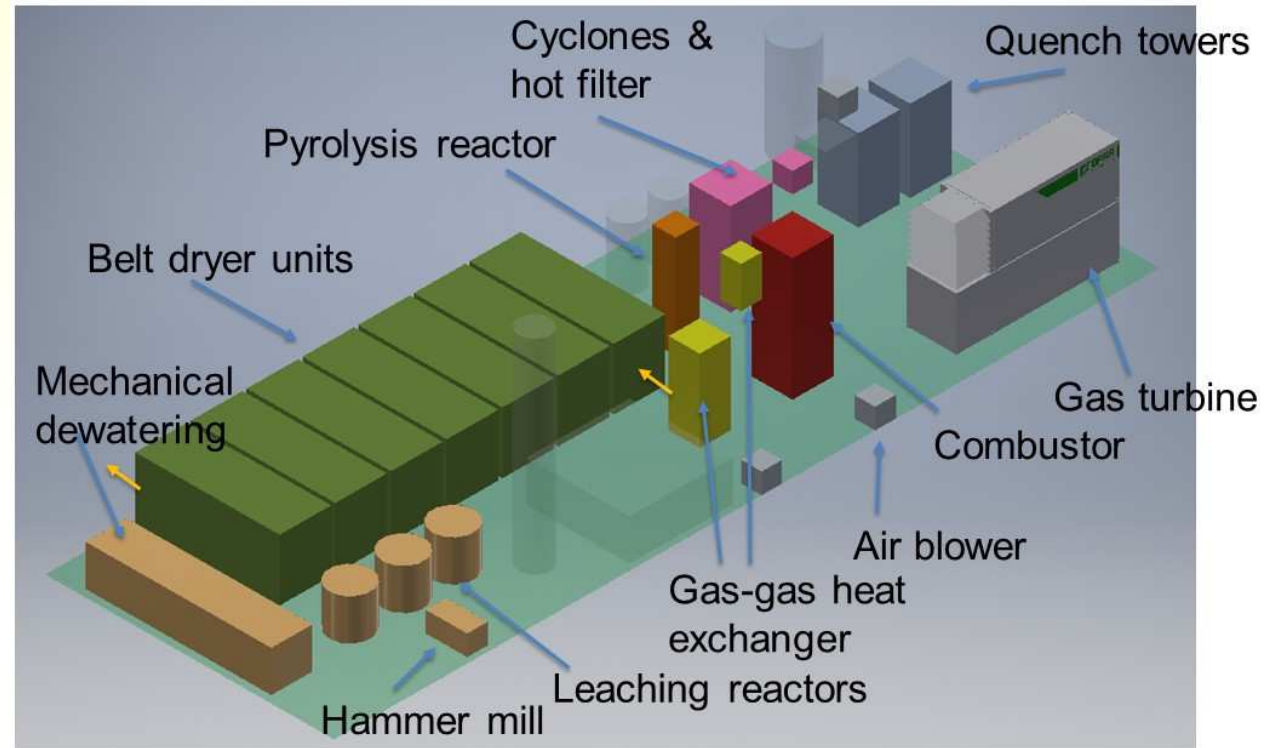
### Efficient combustion of pyrolysis oil in a gas turbine combustor

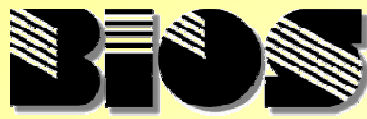
- Efficient combustion of wood pyrolysis oil has been achieved in a full-scale gas turbine combustor
- Low CO levels have been reached over whole load range
- Elevated  $\text{NO}_x$  emissions due to the nitrogen content of pyrolysis oil (0.2 wt%)



Explanation: emissions normalised

- The experimental work performed within the project is in its final phase
- Presently process design and process simulations regarding the overall full-scale EnCat process are on-going
- Process design is accompanied by techno-economic analyses and life-cycle assessments of the whole process chain
- The project shall be finalized in August 2020





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Hedwig-Katschinka-Straße 4, A-8020 Graz

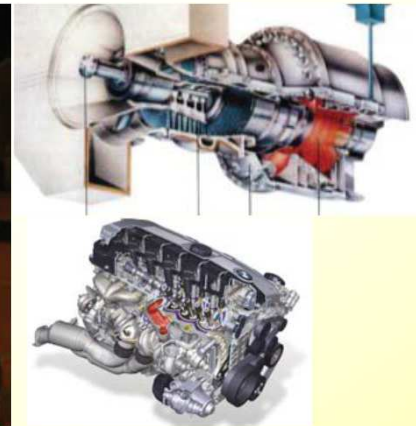


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# Thank you for your attention



**Contact:**

**Dipl.-Ing. Dr. Thomas Brunner**

**Hedwig-Katschinka-Straße 4, A-8020 Graz, Austria**  
**phone: +43 (316) 481300; fax: +43 (316) 4813004**

**Email: [brunner@bios-bioenergy.at](mailto:brunner@bios-bioenergy.at)**

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